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A photograph of an industrial plant at night, showing large cylindrical tanks, complex piping, and scaffolding illuminated by warm lights against a dark sky.

Feedstock Impact on an IGCC Plant with CO₂ Capture

Gasification Technologies Conference

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INTRODUCTION

The prospect of regulating CO₂ emissions places IGCC as the technology of choice for new (stationary) solid fuel power generation:

- CO₂ capture is an integral part of the configuration
- Pre-combustion capture is currently proven/demonstrated technology (unlike post-combustion capture)
- Addition of CO Shift presents no technology challenges
- CO₂ compression is advantaged by reduced pressure ratio
- Majority of uncertainty lies in regulatory/economic aspects of CO₂ transmission and sequestration (i.e. non-technical aspects)

OBJECTIVES

Demonstrate the overall performance of an IGCC plant with CO₂ capture, employing various feedstock, in terms of:

- Net output
- Net heat rate
- % CO₂ Capture
- TIC (relative)
- COE (relative)

Evaluate Gulf Coast vs. Mine Mouth to assess the relative impact of:

- Feedstock transportation cost
- Regional labor rate
- Site conditions

Factors held constant include:

- Plant configuration
- Base load operation
- CO₂ emission level
- Cost estimating basis
- Economic assumptions

FEEDSTOCK COMPARISON

	Ultimate Analysis, A.R. (Wt%)	Petcoke	Pitt #8	Utah Bit.	IL #6	50/50 Lignite - Petcoke	PRB
increasing →	Moisture	6.0	6.8	8.1	14.2	19.8	27.3
← increasing	Carbon	81.8	71.7	69.6	60.1	59.0	51.3
	Hydrogen	3.4	4.8	4.7	4.2	3.0	3.5
	Nitrogen	1.4	1.3	1.2	1.1	1.2	0.7
	Sulfur	6.6	2.9	0.5	3.1	2.8	0.2
	Oxygen	0.2	4.9	9.9	7.8	6.4	12.5
	Ash	0.6	7.6	10.0	9.5	8.1	4.5
← increasing	HHV, A.R. (Btu/lb)	~13,500	~12,950	~11,600	~10,800	~10,400	~8,800

OVERALL DESIGN BASIS

- Integrated ASU (40-50%)
- E-Gas™ gasification - full slurry quench mode
- Single stage CO shift w/ bypass
- 3 column Selexol™ AGR
- 2 x 1 power block
- GTG w/ N₂ dilution plus SG moisturization (achieve blended fuel LHV = 130 Btu/scf)
- STG throttle; 1800 psia/1050 F/1050 F
- Heat sink = wet cooling tower
- CO₂ emission level = 1100 lb/MWh net (NGCC “footprint”)
- CO₂ compression to 2200 psig @ battery limit (no sequestration)

SITE SPECIFIC – DESIGN BASIS

Mine Mouth Cases

Feedstock	Reference Location	Elevation, ft AMSL	Avg. Annual Ambient, F	Distance to GC, miles	Regional Labor Rate [1]
Petcoke	Beaumont, TX	0	59	0	1.0
Pitt #8	Charleston, WV	939	50	911	1.24
Utah Bit.	Provo, UT	4,448	49	1,743	1.15
IL #6	Decatur, IL	679	48	940	1.26
50/50 Lignite -Petcoke	Longview, TX	330	57	201	1.0
PRB	Casper, WY	5,338	40	1,472	1.15

[1] Relative all-in labor rate (base + burden & benefits + construction indirects)

GULF COAST CASES – PLANT PERFORMANCE SUMMARY

	Petcoke	Pitt #8	Utah Bit.	IL #6	50/50 Lignite - Petcoke	PRB
Feed Rate, TPD	4,947	5,256	6,005	6,584	7,038	8,388
Gross Power, MW	729	745	750	757	761	781
Aux Load, MW	159	140	150	154	159	170
Net Power, MW	570	605	600	604	602	611
Net Heat Rate, Btu/kWh (HHV)	9,753	9,412	9,651	9,807	10,224	10,060
% CO ₂ Capture [1]	49.1	42.3	44.8	45.4	47.6	49.0

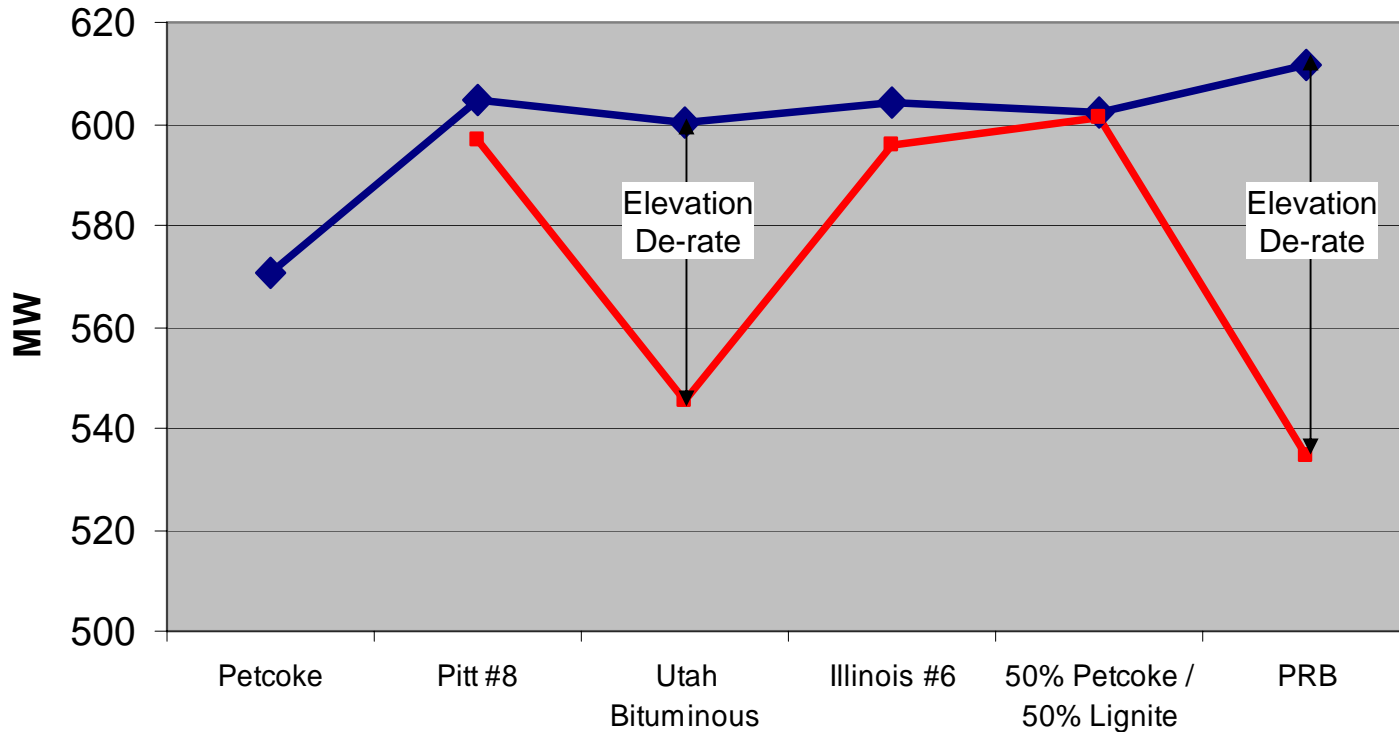
[1] expressed on the basis of combusted carbon in the feedstock @ 1100 lb CO₂ / MWh net

MINE MOUTH CASES – PLANT PERFORMANCE SUMMARY

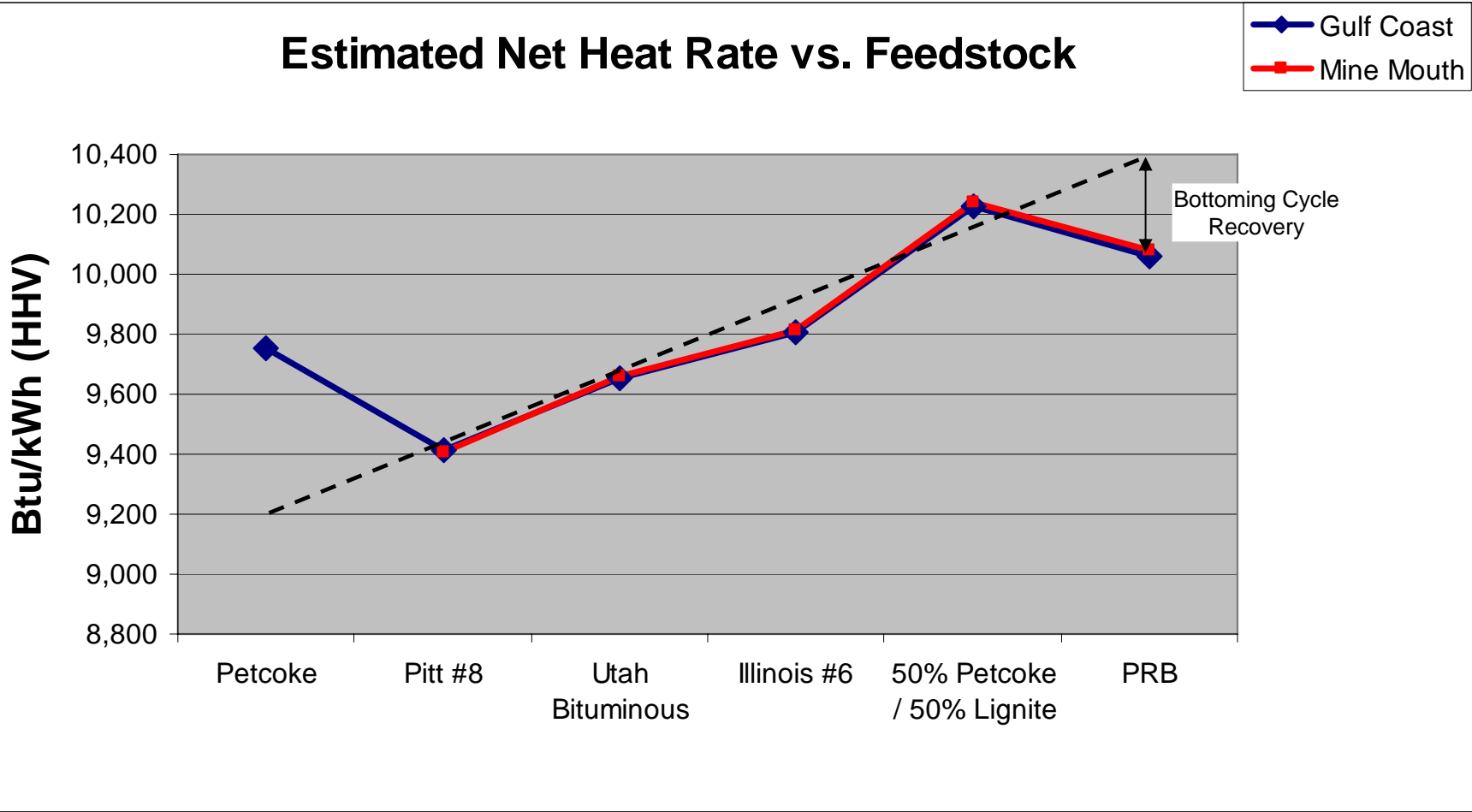
	Pitt #8	Utah Bit.	IL #6	50/50 Lignite - Petcoke	PRB
Feed Rate, TPD	5,182	5,459	6,497	7,034	7,667
Gross Power, MW	735	685	748	761	711
Aux Load, MW	139	138	152	160	160
Net Power, MW	596	546	596	601	551
Net Heat Rate, Btu/kWh (HHV)	9,405	9,657	9,811	10,239	10,196
% CO ₂ Capture [1]	41.9	45.2	45.4	47.6	49.4

[1] expressed on the basis of combusted carbon in the feedstock @ 1100 lb CO₂ / MWh net

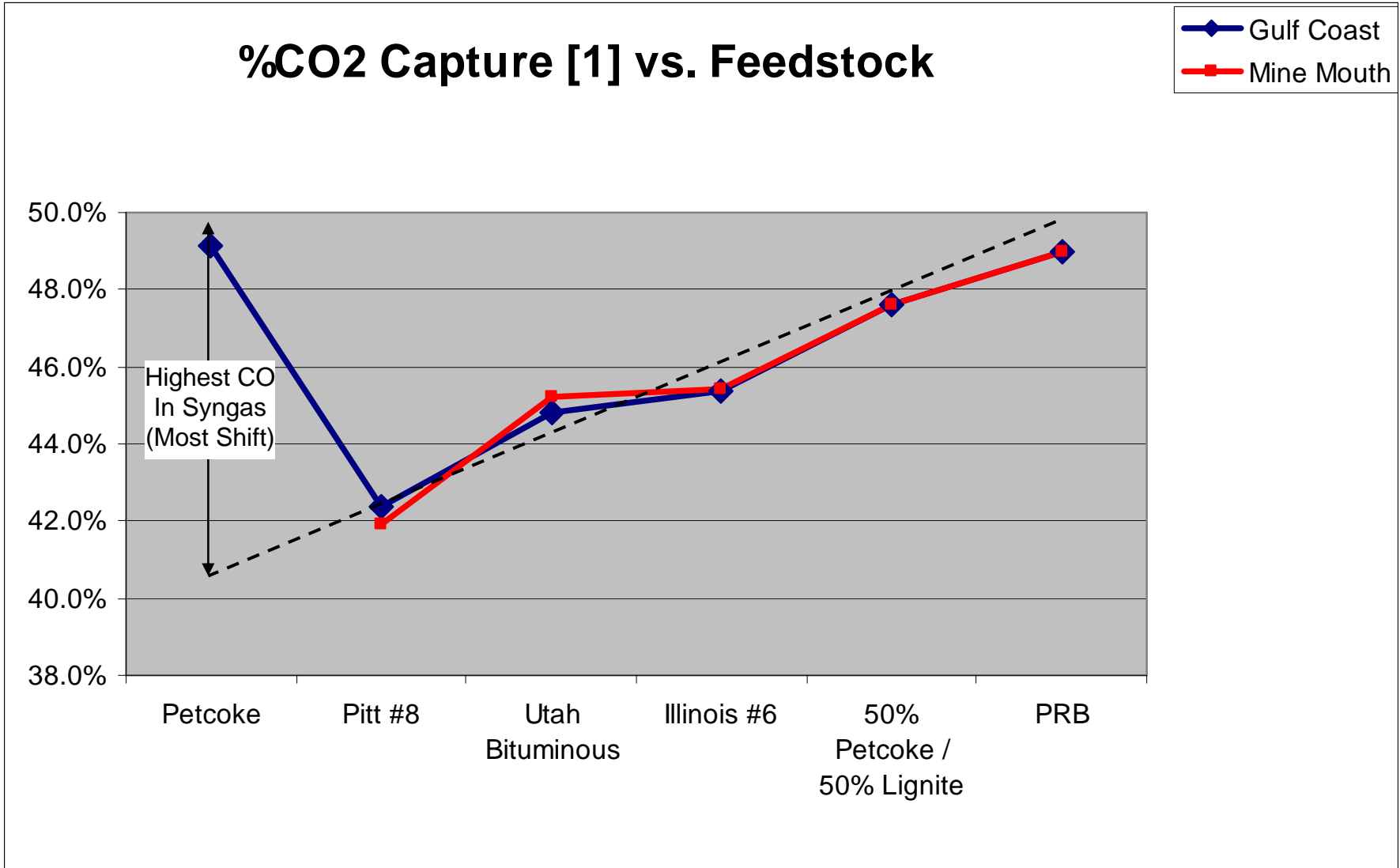
Estimated Net Output vs. Feedstock



Estimated Net Heat Rate vs. Feedstock



%CO₂ Capture [1] vs. Feedstock



[1] expressed on the basis of combusted carbon in the feedstock @ 1100 lb CO₂ / MWh net

ECONOMIC BASIS

Capital Cost

- Equipment & bulks factored @ process block level
- EPC cost including indirects & regional labor rate
- 20% profit & contingency
- Owner's costs including escalation & contingency

Schedule – 5 yr project, COD = 2014

O&M – 4% EPC cost

Financial Assumptions

- COE back-calculated to achieve 10% IRR
- 3% escalation
- 10% interest rate on 100% debt
- Sulfur = \$ 50/ton, no credit for slag
- 37% tax rate

Feedstock

Costs (2008)

Feedstock	Petcoke	Pitt #8	Utah Bit	IL #6	50/50 blend [3]	PRB
\$/ton [1]	\$ 110.00	\$ 141.00	\$ 63.00	\$ 65.00	\$ 21.25	\$ 11.35
\$/MMBtu	\$ 4.07	\$ 5.44	\$ 2.72	\$ 3.01	\$ 1.45	\$ 0.64
\$/ton (delivered) [2]	\$ 116.91	\$ 172.31	\$ 122.90	\$ 97.30	\$ 28.16	\$ 61.93
\$/MMBtu (delivered)	\$ 4.33	\$ 6.64	\$ 5.31	\$ 4.50	\$ 1.92	\$ 3.52

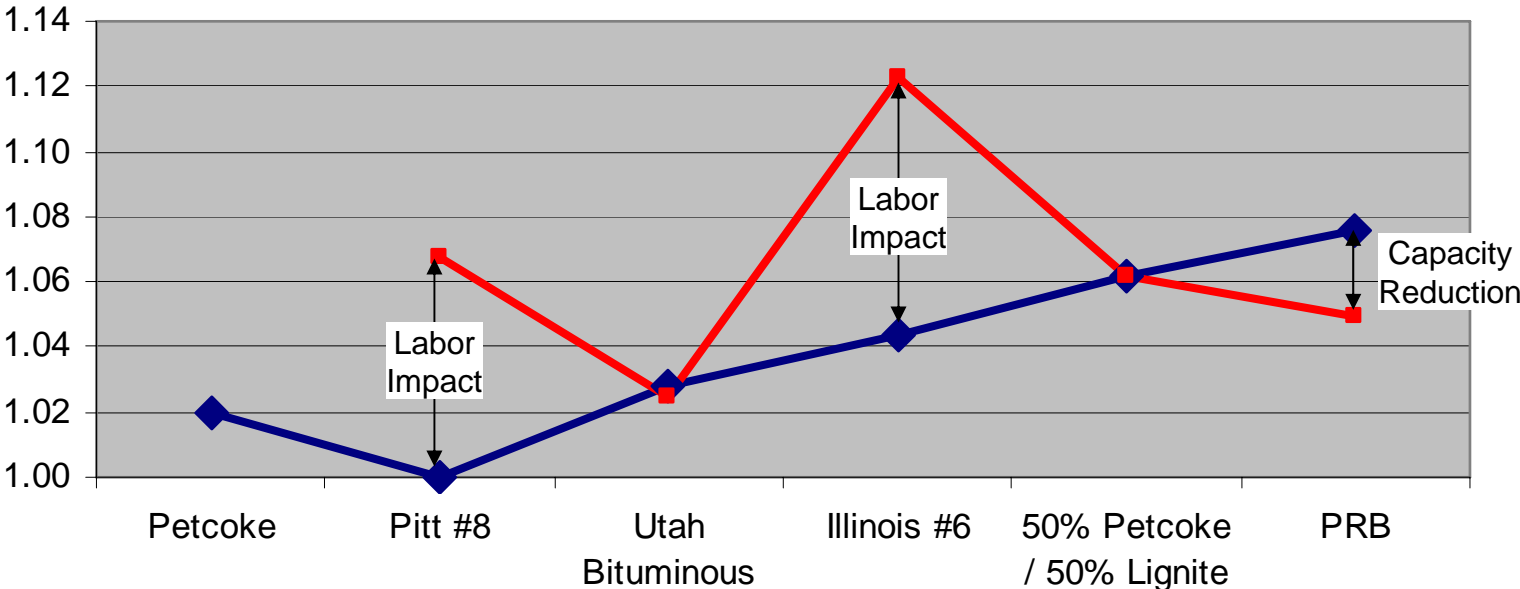
[1] pricing: coal; SNL Energy Coal Report, Lignite; NETL Study 2004 (Contract #DE-AM26-99FT404665)

[2] transportation cost from DOT- BTS Table 3-17 for Class I rail 2006

[3] Lignite component only

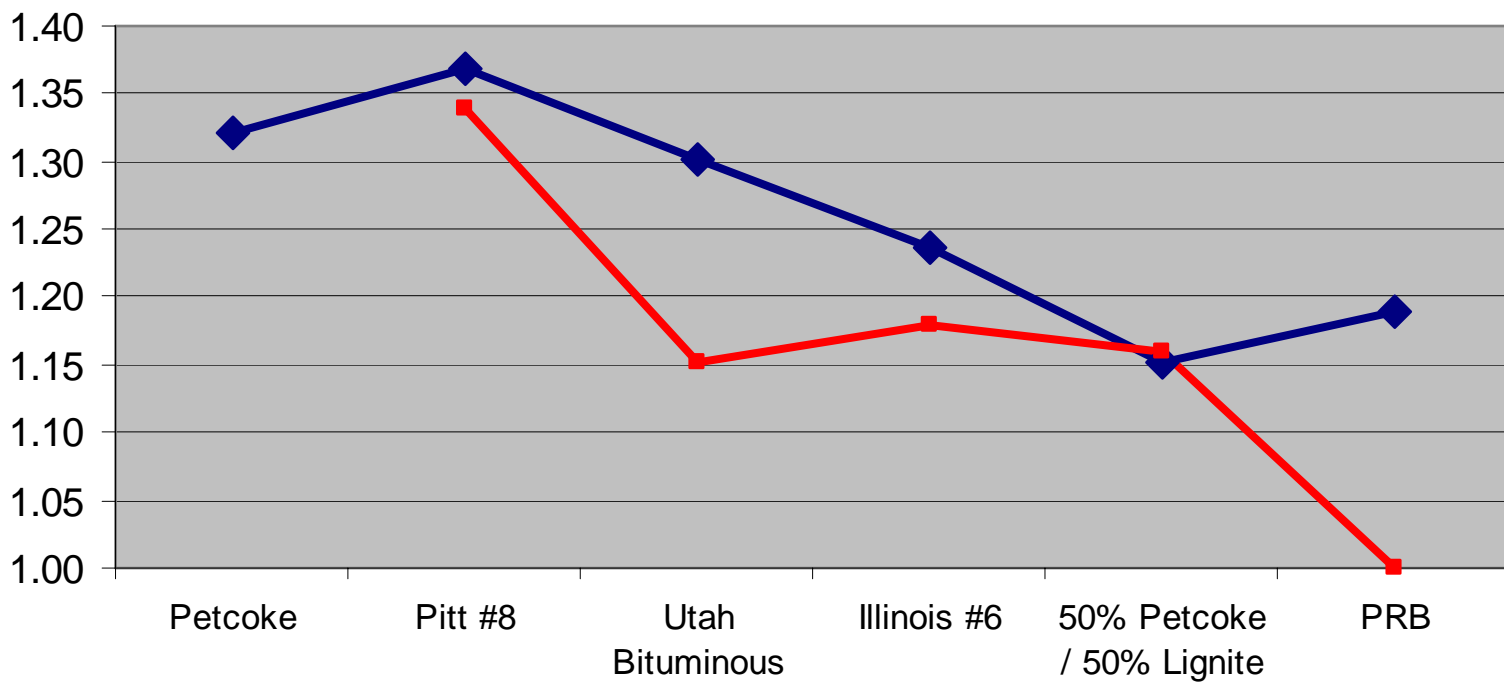
Relative TIC vs. Feedstock

- Gulf Coast
- Mine Mouth



Relative COE vs. Feedstock

◆ Gulf Coast
■ Mine Mouth



CONCLUSIONS

- Transportation cost impact is \geq mine mouth performance impact on COE.
- Feedstock impact on capital cost is \leq 15% across the range at both Gulf Coast and mine mouth locations
- Plant performance trends (power, heat rate) with CO₂ capture are reasonably predictable and rational
- CO₂ capture required to meet the emissions target is highly feedstock dependant, and does not vary appreciably with plant performance at site conditions
- Lower quality feedstock generates lower COE