



# Air Permitting for Gasification and IGCC Plants

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# Topics

- Emission controls for gasification and IGCC
- Applicable regulations for IGCC
- How does IGCC compare to PC and NGCC?
- New Source Performance Standards
- IGCC emission rate comparison charts
- Startup and shutdown emissions

# Air Emissions

# IGCC – Sulfur Removal

- Gasification occurs in a reducing atmosphere (oxygen-starved)
- Sulfur compounds are liberated as  $H_2S$  and  $COS$ , not  $SO_2$
- $H_2S/COS$  removed by refinery industry technologies to levels  $\geq 99\%$
- Recovered as molten sulfur or sulfuric acid
- Sulfur compounds remaining in the syngas are burned in the gas turbine and become low-level  $SO_2$  in the HRSG exhaust



# IGCC – NOx Removal

- Controlled by moisturizing the syngas and injecting N<sub>2</sub> diluent
  - dilutes and cools the flame, and reduces thermal NOx
- CO<sub>2</sub> in the syngas stream also acts as a diluent
- Gas turbines use diffusion burners vs the dry low NOx burners used in NGCC
- SCR is an option for additional NOx removal

# What Regulations Apply to IGCC?

# New Source Performance Standards

- IGCC is covered under Subpart Da as an Electric Utility Steam Generating Unit (just like PC boilers) if:

*“The combined cycle gas turbine is **designed and intended** to burn fuels containing 50 percent (by heat input) or more solid-derived fuel not meeting the definition of natural gas on a 12-month rolling average basis”*

- IGCC gas turbines are not covered by Subpart KKKK, even when natural gas is used

# NSPS for IGCC

<b>Emission</b>	<b>NSPS</b>	<b>NSPS on Gasifier Input Basis (calculated)</b>	<b>NSPS on Gas Turbine Input Basis (calculated)</b>
<b>NO<sub>x</sub></b>	1.0 lb/MWh*	0.143 lb/MMBtu	0.188 lb/MMBtu
<b>SO<sub>2</sub></b>	1.4 lb/MWh* and minimum 95% removal	0.2 lb/MMBtu	0.263 lb/MMBtu
<b>Particulate Matter</b>	Lesser of 0.14 lb/MWh* or 0.015 lb/MMBtu**	0.011 lb/MMBtu	0.015 lb/MMBtu**
<b>Mercury</b>	20 x 10 <sup>-6</sup> lb/MWh*	2.87 lb/TBtu	3.75 lb/MMBtu

\*Output-based standards are on a gross generation basis

\*\* Gas turbine heat input basis, filterable PM only

# Emission Rate Units

- Some IGCC permits list emission rates in lb/MMBtu of gasifier (coal) heat input
- Others list emission rates on gas turbine (syngas) heat input basis (like NGCC)
- EPA addressed this issue:
  - *“The heat input for an IGCC facility is **the heat content of the syngas burned in the stationary combustion turbine and not the heat content of the coal fed to the gasification facility**. The gasification facility is not part of the affected source under subpart Da, only the stationary combustion turbine (turbine and heat recovery steam generator) are covered.”*

# Emission Rate Units

- Permit limits are to be expressed on basis of syngas input to the gas turbine
- Permit applications or permits can list “equivalents” on gasifier input basis, as well as lb/hr and ppm
- Important to specify heat input basis in permit application and in permit

# Permit Limit Units - NOx Example

<b>NOx Emissions from Gas Turbine</b>	<b>Emission Rate Gasifier (Coal) Input Basis</b>	<b>Emission Rate Gas Turbine (Syngas) Input Basis</b>
161 lb/hr	0.059 lb/MMBtu	0.077 lb/MMBtu

30% difference!

# Emission Rate Units

EMISSION UNIT	DESCRIPTION	POLLUTANT	EMISSION LIMITATION BASED ON CT HEAT INPUT	EMISSION LIMITATION BASED ON GASIFIER HEAT INPUT
HRSG1 & HRSG2	Combustion Turbine 1 & 2 (each)	<b>PM<sub>10</sub> filterable</b> (syngas & Natural gas)	0.0085 lb/MMBtu	0.0063 lb/MMBtu filterable (BACT)
		<b>PM<sub>10</sub> Total</b>	0.0217 lb/MMBtu	0.0161 lb/MMBtu Total
		Opacity	20%	20 %
		CO – syngas	0.0485 lb/MMBtu	0.036 lb/MMBtu
		CO - natural gas	0.0449 lb/MMBtu	
		NO <sub>x</sub> syngas	0.0331 lb/MMBtu	0.0246 lb/MMBtu
		NO <sub>x</sub> natural gas	0.0246 lb/MMBtu)	
		SO <sub>2</sub> – syngas	0.0158 lb/MMBtu	0.0117 lb/MMBtu (BACT)
		SO <sub>2</sub> - natural gas	0.001 lb/MMBtu	
		VOC – syngas	0.0015 lb/MMBtu	0.0011 lb/MMBtu
		VOC natural gas	0.0017 lb/MMBtu	
		H <sub>2</sub> SO <sub>4</sub> – syngas	0.0035 lb/MMBtu	0.0026 lb/MMBtu (BACT)
		H <sub>2</sub> SO <sub>4</sub> - natural gas	0.0001 lb/MMBtu	
		Hg – syngas		20 x 10 <sup>-6</sup> lbs/MWh
Hg - natural gas		2.6 x 10 <sup>-4</sup> lbs/MMscf*		

Source: KY DAQ – Cash Creek Generation permit

# Emission Rate Units

**Table A-3. Polk Power Station Unit 6 IGCC; CT/HRSG Emissions (Per CT/HRSG Unit)  
NO<sub>x</sub>, SO<sub>2</sub>, CO, VOC, PM<sub>10</sub>, and Pb Emission Rates - Syngas**

Pollutant	Averaging Period	Units	Operating Case									Maximums
			1 - Syn 0° F Amb. 100% Load	2 - Syn 0° F Amb. 80% Load	3 - Syn 0° F Amb. 60% Load	4 - Syn 59° F Amb. 100% Load	5 - Syn 59° F Amb. 80% Load	6 - Syn 59° F Amb. 60% Load	7 - Syn 100° F Amb. 100% Load	8 - Syn 100° F Amb. 80% Load	9 - Syn 100° F Amb. 60% Load	
Operating Hours	Annual	hrs/yr	8,760	8,760	8,760	8,760	8,760	8,760	8,760	8,760	8,760	8,760
Output <sup>1</sup>	Maximum	MW, gross	413.3	341.4	275.5	408.0	338.8	268.7	398.5	308.4	245.0	413.3
Gasifier Heat Input <sup>2</sup>	Max. Hourly	10 <sup>6</sup> Btu/hr (HHV)	3,200	2,691	2,265	3,073	2,577	2,138	3,047	2,373	1,982	3,200
CT Heat Input	Max. Hourly	10 <sup>6</sup> Btu/hr (HHV)	2,571	2,162	1,820	2,469	2,071	1,718	2,448	1,907	1,593	2,571
NO <sub>x</sub>	30-day	lb / 10 <sup>6</sup> Btu <sup>2</sup>	0.031	0.029	0.028	0.032	0.029	0.028	0.031	0.028	0.028	0.032
		lb / MWh, gross	0.24	0.23	0.23	0.24	0.22	0.22	0.23	0.22	0.22	0.24
	ppmvd @ 15% O <sub>2</sub>	9.1	9.0	9.0	9.0	9.1	9.1	8.6	9.1	9.1	9.1	
	tpy	N/A	N/A	N/A	433.6	N/A	N/A	N/A	N/A	N/A	N/A	433.6
	lb/hr	100	77	64	99	74	60	93	67	55	100	
		g/s	12.6	9.7	8.1	12.5	9.3	7.6	11.7	8.4	6.9	12.6

# Air Emissions

- Same HRSG stack emission points as NGCC
- Same fugitive dust issues as PC
  - Haul roads, coal delivery, unloading and handling
- Similar air permitting requirements
  - Air dispersion modeling
  - BACT analysis
  - Emission controls determination

# Air Emissions

- Unique emission points depend on technology provider
  - Flare
  - Sulfur Recovery Unit tail gas incinerator
  - Sulfuric Acid Plant stack
  - Tank vent incinerators
  - ASU cooling tower



# What About SCR for IGCC?

- Technical issues
  - The fuel is syngas, not natural gas as in NGCC
  - Ammonium sulfate/bisulfate deposit in the HRSG, causing corrosion and plugging, requiring numerous washdowns and downtime
  - No coal-based IGCC system in the world uses SCR
- Economic Issues
  - No commercial guarantees yet with syngas
  - Deep sulfur removal, i.e. Selexol, is required, with higher capital cost than MDEA

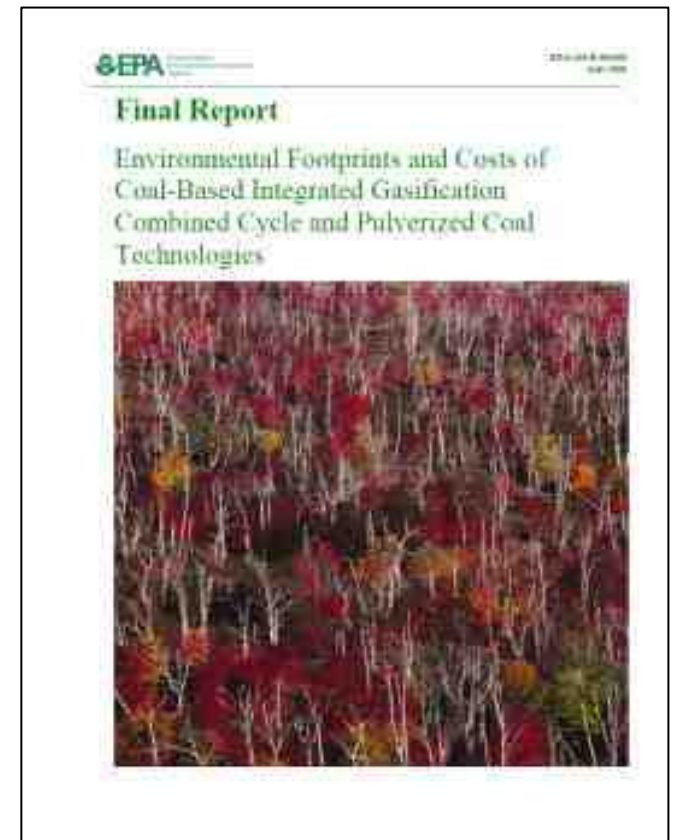


# Why SCR?

- SCR has been proposed for a wide variety of reasons by IGCC applicants:
  - As BACT
  - As Innovative Control Technology to reduce emissions beyond diluent injection
  - As a trial/experiment, with emission limits only for natural gas use
  - To evaluate SCR as part of DOE demonstration program with a syngas-fired combined cycle unit
  - To minimize NO<sub>x</sub> emissions in order to reduce NO<sub>x</sub> emission allowance costs

# NOx BACT

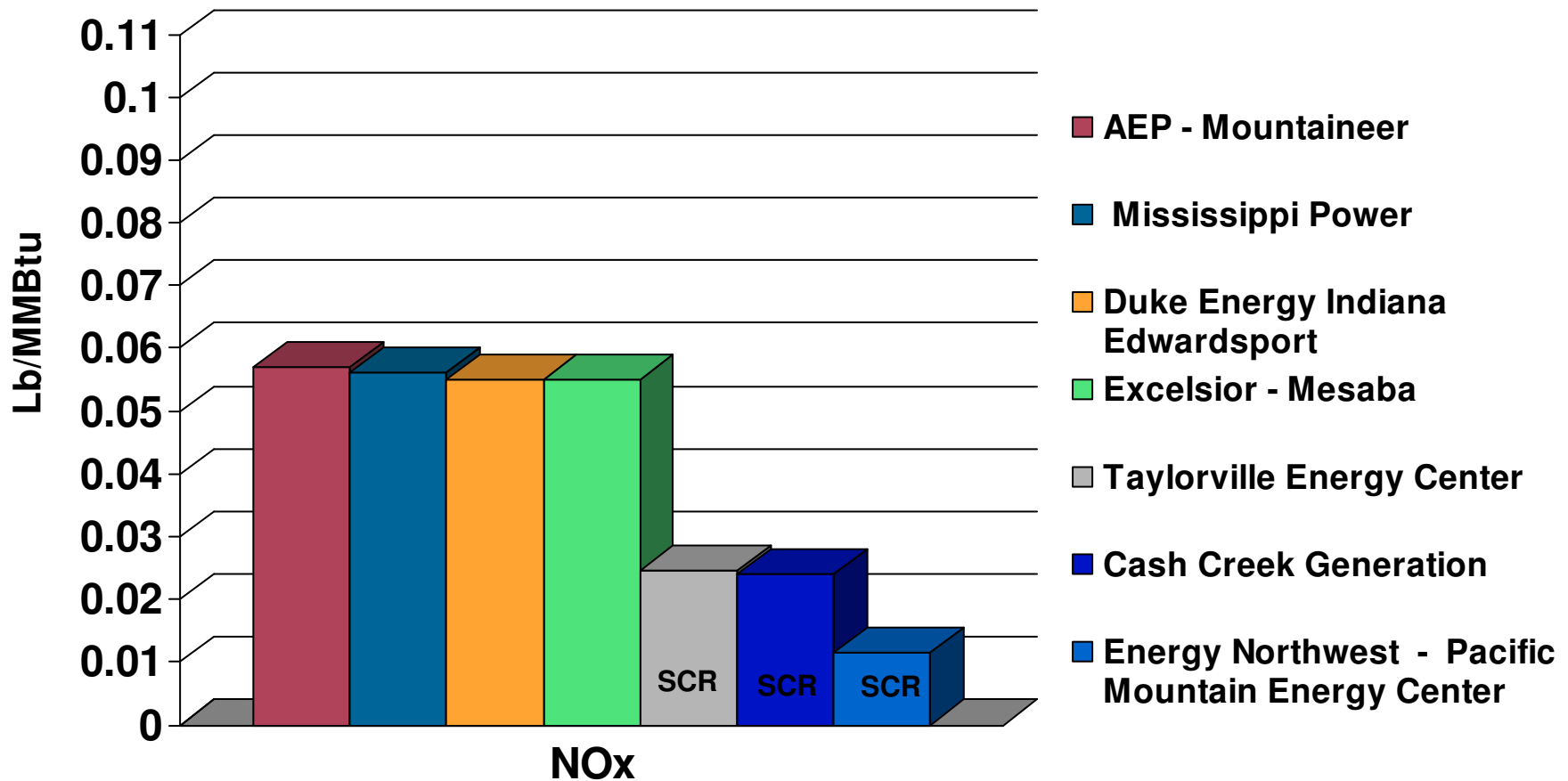
- EPA addressed this in report
- Study notes technical problems with using SCR w/IGCC
- Looked at SCR, w/Selexol for deep sulfur removal
- EPA concluded that:
  - even w/Selexol, problems are not solved
  - additional cost and reduced output are negative impacts to IGCC
  - BACT will continue to be a case-by-case issue



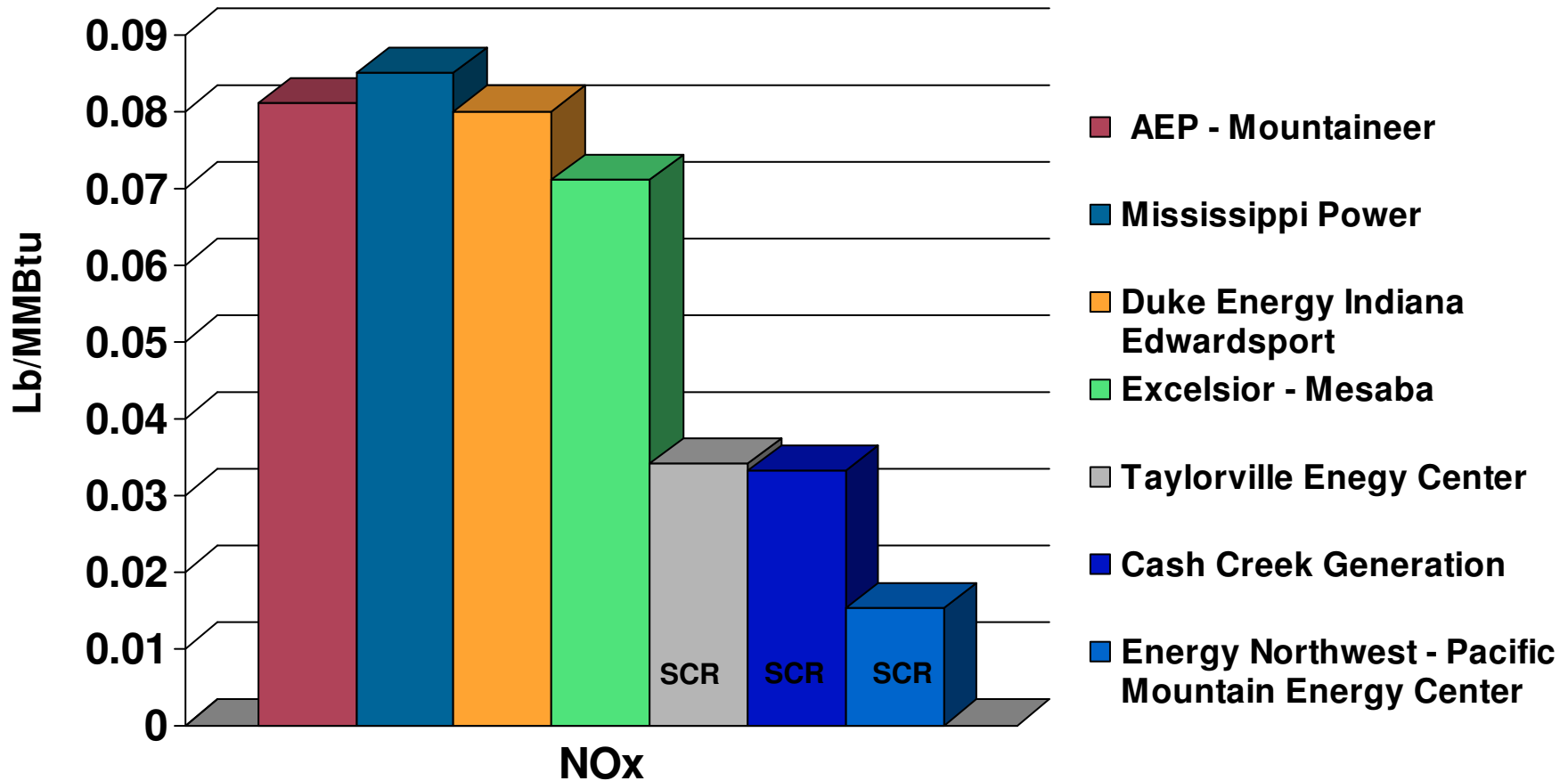
# Permit Limit Comparisons

- Publicly available information
  - Permit applications
  - Draft permits
  - Final permits
  - Submittals to other agencies
  - Some units have been cancelled
- Values are provided on gasifier and gas turbine heat input bases

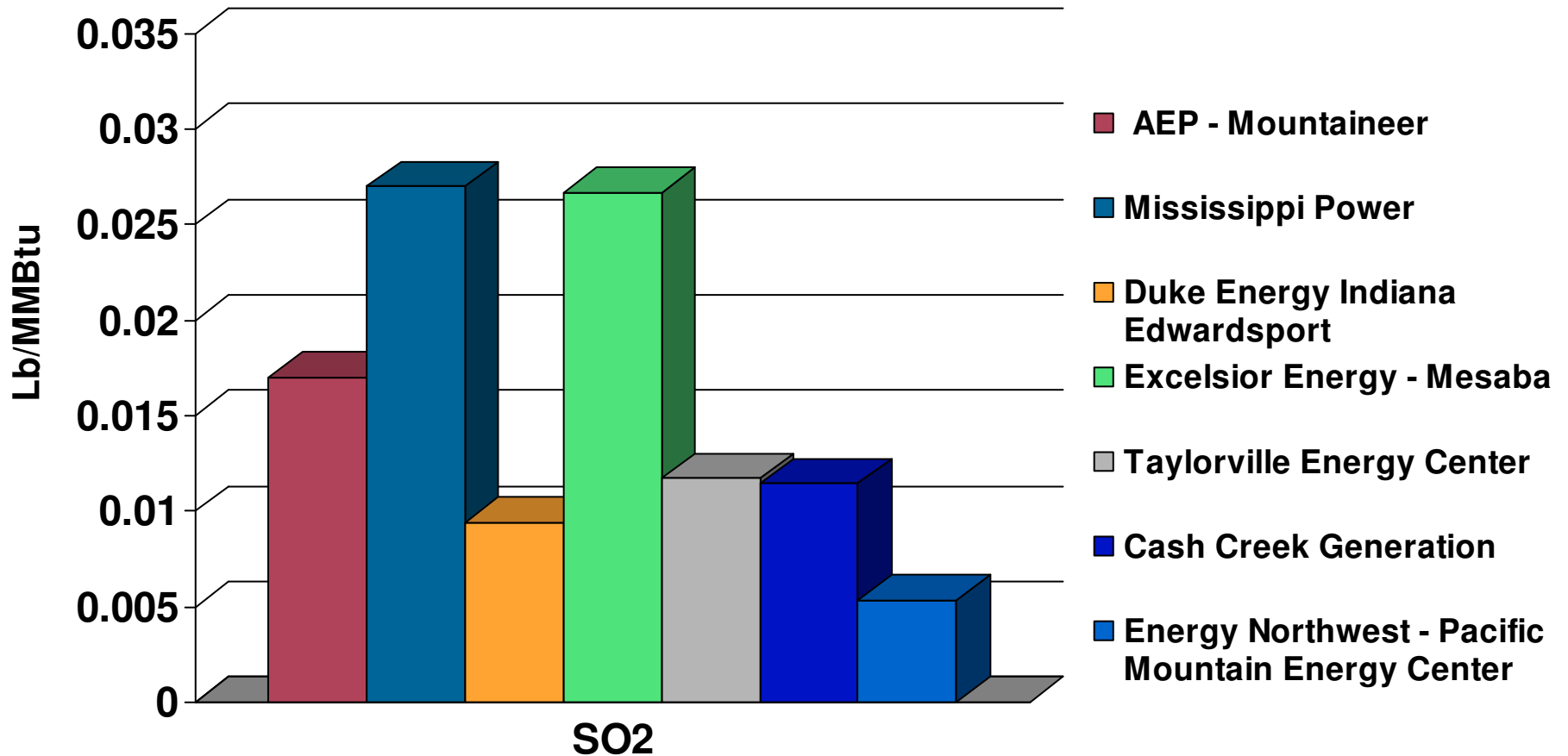
# NOx Emission Rate Comparison Gasifier Heat Input Basis



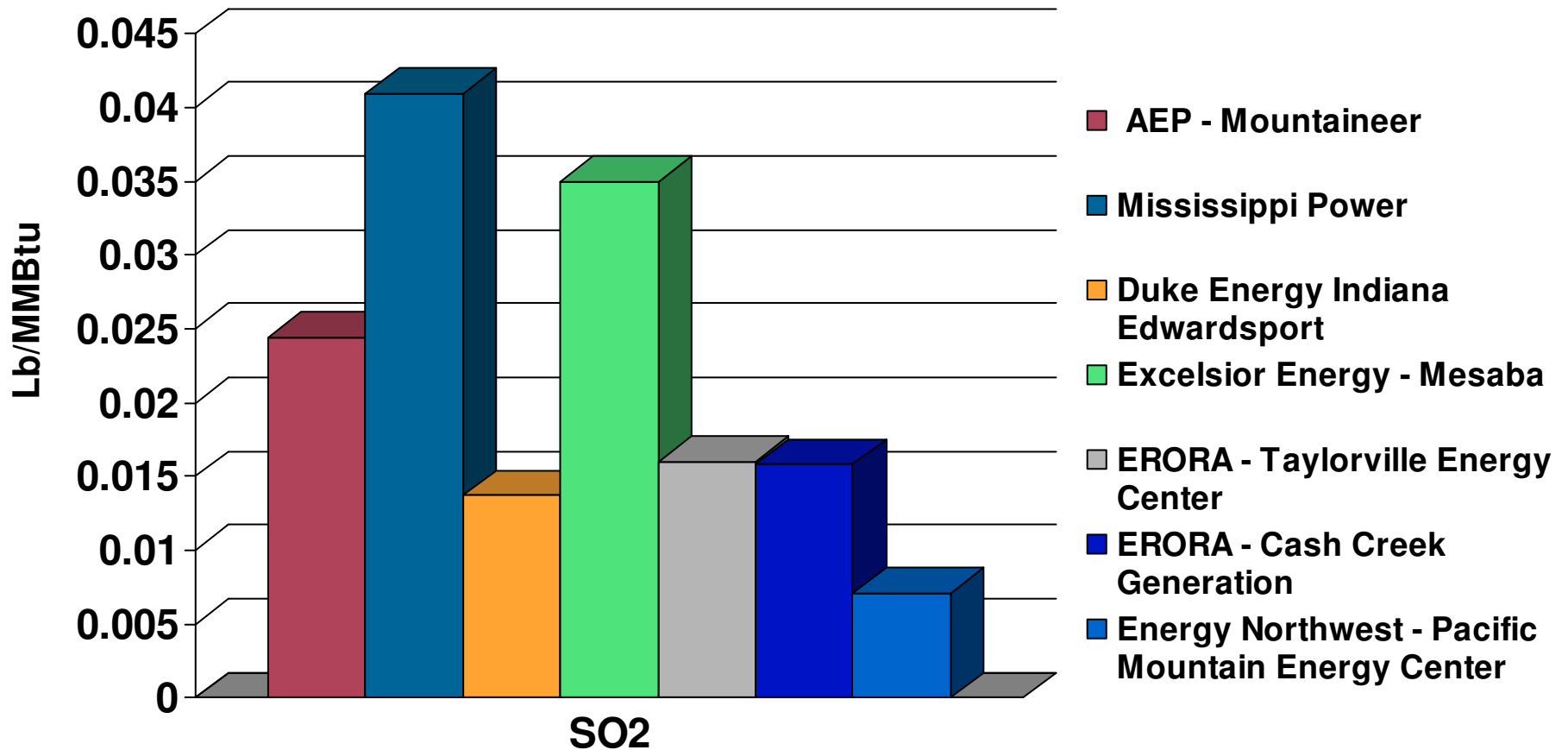
# NOx Emission Rate Comparison Gas Turbine Heat Input Basis



# SO<sub>2</sub> Emission Rate Comparison Gasifier Heat Input Basis



# SO<sub>2</sub> Emission Rate Comparison Gas Turbine Heat Input Basis



# Mercury Removal

- Pre-sulfided carbon beds
- >94% removal of vapor-phase mercury at Eastman Chemical
- Forms a mercury-sulfur complex
- Spent carbon disposed of in drums once/year
- Most IGCC plants plan to use this technology



*Source: Eastman Chemical*

# Start-up and Shutdown Emissions

- Can be a significant source of annual emissions
- Dependent on:
  - Number of start-ups and shutdowns
  - Startup procedures, i.e. starting first gasifier, then second, or both in parallel
  - Startup “fuel”
  - Duration
  - Flaring of raw/treated syngas or acid gas
  - Recycling through acid gas removal system
- Industry has made design and operational enhancements to minimize these emissions

# Questions?

# Contact Info

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